

**Amendment to the Specification:**

Please replace the first paragraph after the title, referencing related applications, on page 1, with the following rewritten paragraph.

This application is a continuation of ~~claims the benefit of~~ U.S. Patent Application No. 09/830,936 filed May 2, 2001, and now U.S. Patent 6,680,361, which is the National Stage of International Application No. ~~claims the benefit of PCT Application~~ PCT/US99/25637, filed November 2, 1999, which claims the benefit of U.S. Provisional Application No. 60/106,569, filed November 2, 1998.

Please replace the paragraph beginning on page 45, line 10, with the following rewritten paragraph.

Product from the first reactor enters the second reactor where it encounters a new set of parameters that includes a flow of gaseous hydrogen (H<sub>2</sub>). The parameters are as follows: C<sub>2</sub> feed rate of 8.2 pph, C<sub>3</sub> feed rate of 3.9 pph, ENB feed rate of 0.03 pph, H<sub>2</sub> feed rate of 364 sccm (0.7 mole% H<sub>2</sub> ~~0.018 mole% H<sub>2</sub>~~, based on moles of fresh H<sub>2</sub> in the feed divided by moles of fresh H<sub>2</sub> in the feed plus moles of fresh C<sub>2</sub> in the feed), reactor temperature of 110°C, catalyst flow rate of 0.41 pph, FAB flow rate of 0.51 pph, MMAO flow rate of 0.48 pph, cocat/Ti ratio of 3.77, Scav/Ti ratio of 4.94, and C<sub>2</sub> conversion of 82.6%. The reactor pressure is the same as in the first reactor. The catalyst efficiency is 0.315 MM# / #. The resulting polymer has a propylene content of 28.1% and an ENB content of 0.55%, both percentages being based on resulting polymer weight, an overall MV of 22.9, an overall M<sub>w</sub> of 109,100, an overall MWD of 2.85, a RR of 42 and a PRR of 36.3. A sample of the polymer solution from the first reactor, upon analysis, shows a PRR of 76 and a MV, extrapolated from M<sub>w</sub>, of 40.